

## Molecular dynamics and phenomenological modeling of experimental diffusivities in supercritical mixtures

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### 1. Introduction

With the chemical industry moving towards a greener future, alternatives to conventional harmful organic solvents are required. Supercritical fluids such as supercritical CO<sub>2</sub> (SC-CO<sub>2</sub>), pure or modified with a cosolvent, are widely used alternatives, especially in processes involving mass transfer, as for example, in extraction, multiphase reactors, and chromatography<sup>1</sup>. In extraction processes, the cosolvent allows to fine tune the solvent affinity towards specific solutes<sup>2</sup>. For more sustainable processes it is of utmost importance to obtain a complete understanding of transport properties, *e.g.*, diffusivities, for a large set of chemical compounds with industrial relevance for optimizing their extraction.

In this work, the diffusivities of gallic acid<sup>3</sup> and eucalyptol<sup>4</sup> in SC-CO<sub>2</sub> modified with ethanol will be presented and extensively analyzed with state-of-the-art phenomenological models, such as the predictive Multi-LSM and the classical Wilke-Chang<sup>5</sup> equations. These data will be further compared with diffusivities calculated from trajectories derived from classical molecular dynamics (MD) simulations.

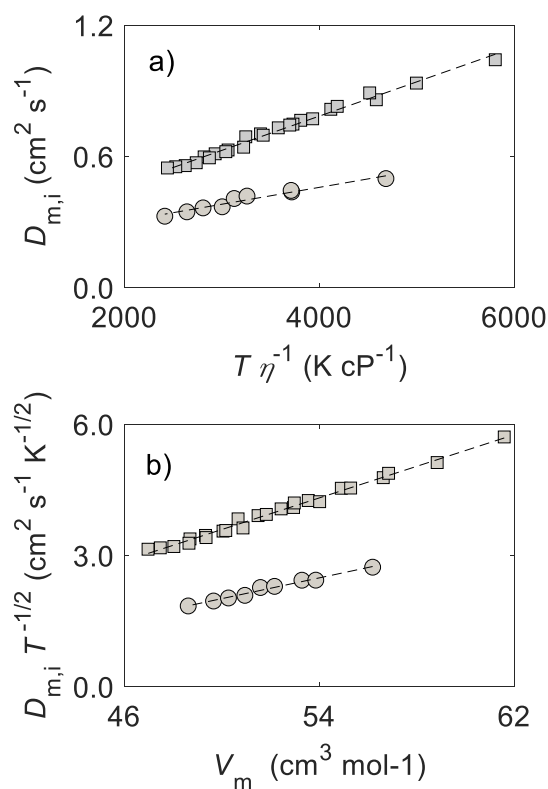
### 2. Materials and Methods

The experimental  $D_{m,i}$  measurements were carried out using the well-known chromatographic peak broadening (CPB) method<sup>6</sup> between 303.15 K and 333.15 K, and from 150 bar to 275 bar. Both gallic acid and eucalyptol were measured in SC-CO<sub>2</sub> modified with ethanol. Molar fractions of 16 mol.% or 8 mol.% of ethanol were used for gallic acid and eucalyptol, respectively.

The MD simulations have been carried with the general-purpose simulation software package GROMACS<sup>7</sup>, using the canonical ensemble (NVT), which considers constant number of molecules,  $N$ , temperature,  $T$ , and system volume,  $V$ . The Elementary Physical Model (EPM2) force field was used for SC-CO<sub>2</sub> while the remaining species considered the optimized potentials for liquid simulation – all atoms (OPLS-AA) parameters. The  $D_{m,i}$  was computed from the long-time limit of the mean square displacement obtained by the Einstein relationship.

### 3. Results and discussion

The experimentally determined  $D_{m,i}$  values of gallic acid in CO<sub>2</sub> modified with 16 mol.% ethanol at  $T = 313.15 - 333.15$  K and  $P = 150 - 250$  bar were between  $3.3 \times 10^{-5}$  cm<sup>2</sup> s<sup>-1</sup> and  $5.0 \times 10^{-5}$  cm<sup>2</sup> s<sup>-1</sup>. As for eucalyptol in SC-CO<sub>2</sub> modified with 6 mol.% ethanol at  $T = 303.15 - 333.15$  K and  $P = 150 - 250$  bar the  $D_{m,i}$  values were in the range  $5.5 \times 10^{-5} - 1.0 \times 10^{-4}$  cm<sup>2</sup> s<sup>-1</sup>. The dependencies on temperature, pressure, free-volume, and Stokes-Einstein coordinates were analyzed for both systems (Figure 1). The data were modeled with the previously mentioned equations, and the average absolute relative deviation (AARD) achieved for the Wilke-Chang model was 156.42 % for gallic acid and 5.31 % for



**Figure 1.** Stokes-Einstein (a) and free-volume representations (b) of gallic acid (●) and eucalyptol (■) diffusivities in supercritical mixture of CO<sub>2</sub> and ethanol.

eucalyptol. As for the Multi-LSM, the AARD values were lower than the ones achieved by the Wilke-Chang equation, with values of 23.14 % and 3.02 % respectively.

Regarding MD simulations, they have been carried out at the limit conditions of the experimental measurements in order to validate a newly developed procedure for  $D_{m,i}$  estimation in supercritical mixtures of CO<sub>2</sub> and ethanol.

#### 4. Conclusions

Experimental diffusivities of gallic acid and eucalyptol in CO<sub>2</sub> modified with ethanol under supercritical conditions have been successfully measured using the CPB method. The data was modelled with the Multi-LSM and Wilke-Chang equations. For the eucalyptol diffusivities, the results achieved by both equations were equivalent while in the case of the gallic acid there is a clear advantage in using the Multi-LSM equation despite being more complex. The MD simulations attained good results, being a successful tool for the computer calculation of these diffusion coefficients in alternative to the phenomenological models.

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